

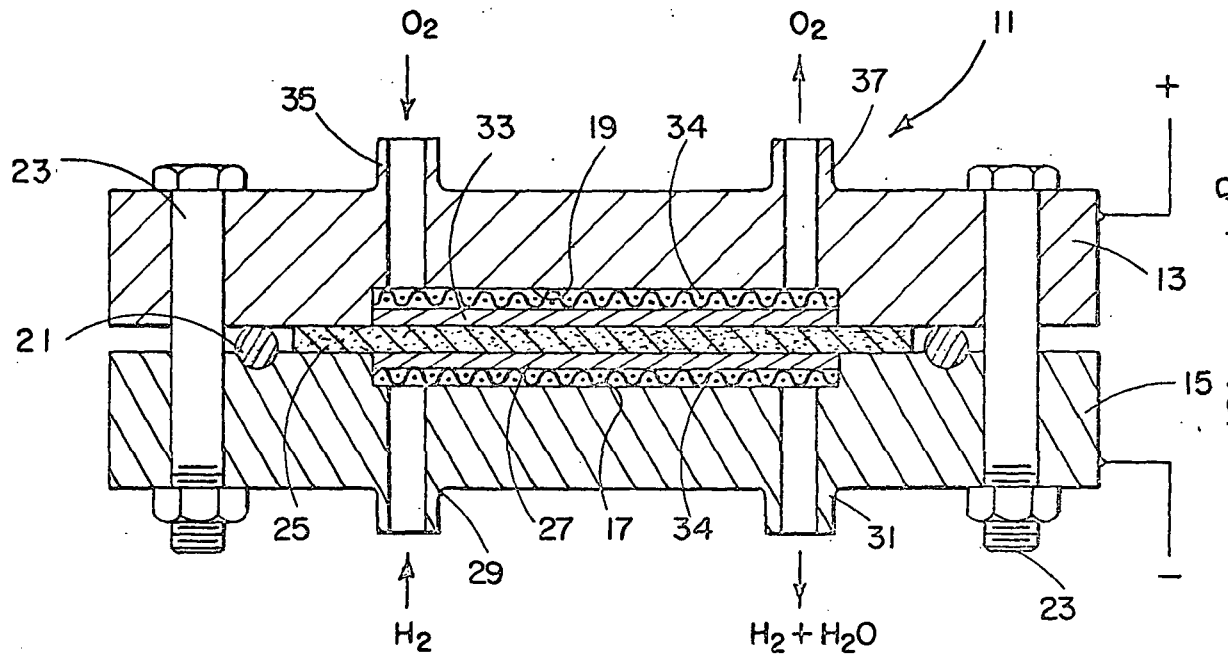
NASA CASE NO. *7497-10537-1*
PRINT FIG. *The Figure*
N72-10138

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N72-10138 4020

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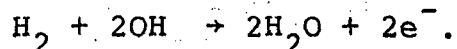
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Inventor: Larry Leroy Swette NASA Case HQN-10537-1
Contract NASw-1233
Contractor: Tyco Laboratories, Inc. December, 1970

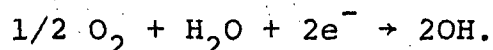
ELECTROCATALYST FOR OXYGEN REDUCTION

The object of this invention is to provide a new catalyst composition useful for electrochemical oxygen reduction in low temperature alkaline fuel cells. Further, an object of the invention is to provide a catalyst which has improved properties over those previously utilized, as well as being less expensive.

The figure discloses a typical alkaline fuel cell for the electrochemical oxygen reduction. As seen in the figure, the fuel cell 11 contains cell plates 13 and 15 which have cavities 17 and 19 formed at the centers thereof. An O-ring seal 21 surrounds the cavities. Disposed between the plates is an electrolyte 25 containing an aqueous solution of potassium hydroxide in a suitable matrix. On one side of the electrolyte is a hydrogen oxidation anode 27 of conventional construction such as platinum black dispersed in a binder therefor. The anode 27 is maintained in place by screens 34. Hydrogen is directed through an inlet 29 and exits through line 31. Disposed on the opposite side of the electrolyte is the oxygen reduction electrode 33 of this invention which is comprised of a mixture of platinum and silver dispersed in a suitable inert binder such as tetrafluoroethylene. The catalytic mixture will contain from 20 to 40 atomic percent platinum with the remainder being silver. An inlet 35 directs oxygen gas to cavity 19 while exit line 37 will conduct excess oxygen. The reaction of the above described fuel cell involves in the anode



At the cathode of the cell, the reaction is



A preferred composition for the catalyst of this invention is 30 atomic percent platinum with the remainder silver. Thus a typical electrode having a loading of 20 mg/cm² of catalyst, would have a platinum loading of 8.6. Such an electrode will provide better performance than a similar one having a platinum loading of 20 mg/cm² and performance equivalent to available electrodes having a platinum loading of 40 mg/cm². Thus it can be seen that the herein catalyst will contain significantly less platinum than previous electrodes while providing superior results.

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Serial No. 112,366
Filed: February 3, 1971

Serial No. 112,366
Filed: February 3, 1971

TYCO Laboratories, Inc.
Contract NASw-1233

S P E C I F I C A T I O N

TO ALL WHOM IT MAY CONCERN:

BE IT KNOWN THAT, Larry Leroy Swette, a citizen of the United States of America, residing at Belmont, in the County of Middlesex, State of Massachusetts, has invented a new and useful

ELECTROCATALYST FOR OXYGEN REDUCTION

of which the following is a specification.

ABSTRACT OF THE DISCLOSURE

A catalyst composition useful for electrochemical oxygen reduction in low temperature alkaline fuel cells comprised of platinum and silver which are dispersed in a resinous inert binder to provide a cell electrode.

ORIGIN OF THE INVENTION

The invention described herein was made in the performance of work under a NASA contract and is subject to the provisions of Section 305 of the National Aeronautics and Space Act of 1958, Public Law 85-568 (72 Stat. 435; 42 USC 2457).

BACKGROUND OF THE INVENTION

1. Field of the Invention

This invention is in the field of fuel cells. More particularly the invention relates to an electrode composition useful in oxygen reduction in low temperature alkaline fuel cells.

2. Description of the Prior Art

Pure platinum catalysts have been considered as the best catalysts for electrochemical oxygen reduction in low temperature alkaline fuel cells. However, pure platinum catalysts are expensive due to the high cost of the material. Further,

1 the pure platinum catalysts have exhibited structural problems
2 indicated by drastic voltage loss at some limiting or high
3 current density.

4 Thus it is an object of this invention to provide an
5 improved catalyst for electrochemical oxygen reduction as
6 compared to a pure platinum catalyst.

7 Another object of this invention is to provide a less
8 expensive catalyst than a pure platinum catalyst for electro-
9 chemical oxygen reduction.

10 SUMMARY OF THE INVENTION

11 The above and other objects of the invention are
12 accomplished by a novel catalyst composition which is comprised
13 of 20 to 40 atomic percent platinum with the remainder being
14 silver. The platinum and silver is in powder form and mixed
15 with a suitable binder, polytetrafluoroethylene. The resulting
16 electrode is formed by pressing the material together, drying
17 it, and then heating it to a point sufficient to sinter the
18 binder. The formed electrode is at least as active as one
19 containing only platinum and is structurally superior to platinum
20 for high current density operation. It is believed the invention
21 will be further understood from the following detailed description
22 and drawings in which

23 BRIEF DESCRIPTION OF THE DRAWINGS

24 The figure represents a cross sectional view of an
25 alkaline fuel cell incorporating the catalyst of this invention.

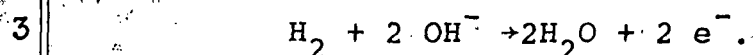
26 DESCRIPTION OF THE PREFERRED EMBODIMENTS

27 Turning to the figure, there is an illustration of a
28 type of fuel cell in which the catalyst electrodes of this
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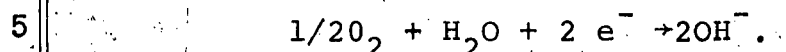
1 invention are typically utilized. The fuel cell 11 is comprised
2 of cell plates 13 and 15. The plates have cavities 17 and 19
3 respectively formed at the center thereof and facing each other.
4 The o-ring seal 21 circumferentially surrounds the cavities 17
5 and 19 and is held in place by bolts 23 that secure the two
6 cell plates 13 and 15 together. Disposed between the two plates
7 is an electrolyte 25. The electrolyte can be of a conventional
8 material such as a 35 weight percent KOH in an aqueous solution
9 in an asbestos matrix. The cell will typically contain a hydrogen
10 oxidation electrode 27 which once again can be of a conventional
11 construction such as a tetrafluoroethylene bonded platinum black
12 material having a loading of 40 mg/cm^2 of platinum on a nickel
13 screen. The electrode 27 is disposed adjacent the electrolyte
14 matrix 25 and held in place by screens 34 or expanded metal
15 structures. This leaves the gas cavity 17 to which an inlet 29
16 and separate outlet 31 are connected. Hydrogen is directed through
17 the inlet 29 and exits through line 31. This results in plate 15
18 being the anode or negative plate of the cell as will be further
19 explained. Disposed on the opposite side of the electrolyte 25
20 from the hydrogen anode is the oxygen reduction electrode 33 of
21 this invention. The electrode 33 will be comprised as will be
22 further described with a mixture of platinum and silver on a
23 suitable screen utilizing an inert binder such as tetrafluoroeth-
24 ylene.

25 An inlet 35 directs oxygen gas to the cavity 19 adjacent
26 the oxygen reduction catalytic surface 33. An exit line 37 from
27 the cavity 19 will conduct excess oxygen from the fuel cells on
28 the oxygen cathode side thereof. This results in plate 13 becoming
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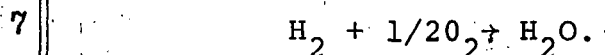
1 the cathode or positive plate of the fuel cell. The reaction in
2 the above described fuel cell involved at the anode is



4 In the cathode of the cell, the reaction is:



6 The overall reaction in the fuel cell is:



8 As indicated, the herein invention is particularly
9 directed to the oxygen reduction catalyst to be used in the
10 electrode 33 of the alkaline fuel cell. Previous to the herein
11 invention, pure platinum catalysts were utilized. Such a pure
12 platinum catalyst was comprised of pressing platinum powder
13 on a suitable screen such as a nickel screen and bonding the
14 powder with an inert resin such as tetrafluoroethylene or the
15 like. The typical loading of the platinum was in the range of
16 10 mg/cm² to 40 mg/cm². It is believed that a particular
17 structure is required for optimum mass transfer of reactants
18 and products to and from catalytic sites on electrode structures.
19 This relates to pore size, particle size and wetting properties
20 of the structure. This is achieved by balancing the relative
21 amounts of binder and catalyst present in the structure.

22 The purpose of the herein invention is to provide a
23 catalyst composition that is at least as active as the pure
24 platinum one, yet contains less platinum. This results in lower
25 costs, as well as providing superior structural properties at
26 high current density operations.

27 The electrode of the herein invention comprises a
28 mixture of platinum and silver with the silver constituting more than
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1 half of the catalyst composition on an atomic percent basis.
2 Thus the catalyst composition utilized in this invention will
3 comprise from 20 to 40 atomic percent platinum with the remainder
4 being silver. To indicate the superiority of this composition
5 as an oxygen reduction catalyst, in an electrode having a
6 loading of 20 mg/cm^2 of catalyst where the atomic ratio of
7 platinum to silver is 30:70 there is present 8.6 mg/cm^2 of
8 platinum. Such an electrode containing this amount of platinum,
9 8.6 mg/cm^2 , provides better performance than a similar electrode
10 with a platinum loading of 20 mg/cm^2 and performance equivalent
11 to available electrodes having a platinum loading of 40 mg/cm^2 .
12 At higher current densities, above 100 ma/cm^2 , less polarization
13 is observed with the catalyst of this invention than is
14 observed for pure platinum electrodes. Thus it can be seen
15 that the herein catalyst at the same loading of catalyst in
16 an electrode will contain significantly less platinum than
17 heretofore has been used yet will produce improved results.

18 In forming the electrode of the invention, platinum
19 powder, preferably platinum black powder, is blended with the
20 silver powder utilized. In practicing the invention, it is
21 preferred to utilize silver oxide rather than pure silver
22 powder. The amount of silver required in the catalyst mixture
23 is then calculated on the basis of the silver present in the
24 silver oxide. The reason for preferring silver oxide is that
25 pure silver powder does not have a very high surface area.
26 Therefore, it is not as catalytically reactive as desired.
27 Further, since silver is very malleable it tends to form a thin
28 foil when subjected to rolling fabrication processes used to
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1 make the electrodes. On the other hand, silver oxide is not
2 malleable and sinters to a much lesser extent during this
3 operation forming the electrode. Further, the silver oxide
4 has a much finer particle size than typical silver powders.

5 After blending the platinum with the silver oxide
6 powder, a dispersion of a binder in a large quantity of water
7 is added to the powder and blended thoroughly. A typical
8 preferred binder is tetrafluoroethylene. The excess water is
9 evaporated from the mixture until the mixture has a consistency
10 approximating modeling clay or dough. This doughy mixture is
11 then rolled onto a suitable expanded metal type screen which,
12 for example, can be of nickel, which is gold plated. Such a
13 screen is typically used for electrodes. The material is rolled
14 on to the screen between two thin sheets of inert plastic
15 material such as tetrafluoroethylene films. The formed electrode,
16 which is dried, is then heated at a much higher temperature to
17 sinter the binder material.

18 In addition to utilizing the foregoing mixed powders to
19 form the electrodes, it is possible to melt a platinum-silver
20 alloy at the proper composition and forming the required powder,
21 for example, by an exploded wire technique or plasma torch
22 vaporization condensation method. Platinum-silver compositions
23 have, for example, previously been made by the Bureau of Mines.

24 In formulating the foregoing electrode the binder
25 weight percent can range from 15 to 40 percent with the remainder
26 being the catalyst. As has been indicated, it is preferred
27 that an inert resinous material be utilized as a binder. Parti-
28 cularly preferred is polytetrafluoroethylene. In addition to
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1 this material, chlorotrifluoroethylene polymers and ethylene/
2 vinyl acetate copolymers such as the Elvax polymers made
3 by E. I. du Pont de Nemours can be utilized as binder materials.
4 During the heating operations, the binder material, such as
5 polytetrafluoroethylene is sintered and the wetting agents used
6 to form the dispersion of the resin in water are driven off.
7 As an initial side effect, some of the silver oxide, if such is
8 used, is probably reduced to silver and partially sintered.
9 The remaining silver oxide is reduced electrochemically to
10 silver during fuel cell operation.

11 The resulting catalyst and electrode formed therefrom
12 is better than an electrode that is obtained with either
13 platinum or silver alone. For example, pure silver electrodes
14 do not show as good a performance for the same loading. Further,
15 a lightweight electrode, which is formed using silver alone
16 loses performance due to sintering which occurs during the
17 fuel cell operation. The initial previous opinion was that
18 platinum is a very good catalyst with a poor structure. However,
19 subsequent theoretical studies indicate that in a tetrafluoro-
20 ethylene bonded electrode, for example, agglomerates existing
21 in platinum black have an ideal structure to make such a
22 tetrafluoroethylene bonded electrode. However, it appears that
23 platinum may be intrinsically less catalytic for oxygen reduction
24 than silver. Thus it appears that the platinum in the electrode
25 in this invention plays primarily a structural forming role
26 while the silver is a catalyst or at least increases the cata-
27 lytic activity of platinum. In other words, the two materials
28 peculiarly enhance each other to make both a better structural
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1 electrode and one having improved catalytic properties at the
2 same loading levels of either platinum or silver alone.

3 It should be pointed out that in order to obtain the
4 same performance as achieved herein with platinum alone, one
5 must utilize, as previously mentioned, a much higher platinum
6 loading and thus incur a much higher price. In addition, an
7 increase in platinum loading does not necessarily mean an
8 equivalent increase in current at a given voltage, because the
9 catalyst utilization becomes poor with increased loading due
10 to the ohmic iR drop across the electrode. Eventually, if
11 the electrode becomes too thick, the catalyst on the back of
12 the electrode is not utilized at all. Thus, further additions
13 of catalyst do not in any way improve performance above a
14 certain limit or thickness. It is believed that the invention
15 will be further appreciated from the following detailed
16 examples.

17 EXAMPLE

18 A low temperature alkaline fuel cell was constructed
19 in accord with that shown in the figure. A circular electrode
20 having an area of 50 centimeters squared was prepared by
21 depositing the catalyst on a gold plated expanded metal type
22 nickel frame. The catalyst was prepared by blending 430 mg
23 of platinum black with 612 mg of silver oxide, which was
24 equivalent to 570 mg of silver. 250 mg of tetrafluoroethylene
25 solids dispersed in water was added to the mixture of powder
26 together with a large quantity of water which was then blended
27 thoroughly. The excess water was evaporated until the mixture
28 had a consistency of modeling clay and was then rolled onto
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1 the screen between two tetrafluoroethylene films. The electrode
2 was then dried at 30°C and sintered in a nitrogen atmosphere
3 oven for 15 minutes at 275°C. This provided an electrode having
4 a platinum to silver ratio of 30 to 70 atomic percent. The
5 resulting tetrafluoroethylene bonded electrode had a loading
6 of 20 mg/cm² or 8.6 mg of Pt/cm². In testing the formed
7 electrode, 35% KOH solution was used in a 30 mil asbestos
8 matrix. The temperature of the cell was 80°C. The hydrogen
9 anode was an American Cyanamid AB-40 anode. The duration of
10 the test was 2275 hours. The electrode of the invention
11 supported a current density of 100 ma/cm² at 930 mv and 140 ma/cm²
12 at 915 mv vs. hydrogen anode. The foregoing performance was
13 obtained with a pure platinum catalyst in the same cell utilizing
14 a loading of platinum of 40 mg/cm². Thus it can be seen that
15 to obtain the equivalent performance, one had a much higher
16 total loading of catalyst, namely 40 mg vs. 20 of the herein
17 catalyst mixture and more particularly contained about four
18 and a half times as much platinum as used in the catalyst of
19 this invention.